

## **Carbon2Chem®**

# L-V Carbon2Polymers: **CO Conversion to Polycarbonates**

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The aim of subproject L-V is to investigate the reaction of CO gas from a steel mill with Cl<sub>2</sub> for producing polycarbonates via phosgene as a key intermediate (Fig. 1). We investigate the interaction of Cl<sub>2</sub> with commercial activated carbons at different temperature via tracking formed gaseous products to draw structure-activity relationships. In close cooperation, the solvent-free phosgenation of phenol and life cycle assessment test is carried out at Covestro and RWTH Aachen, respectively.

### **EXPERIMENTAL APPROACH**

Cl<sub>2</sub> activation is a crucial step for phosgenation. The interaction must not be too strong, otherwise, Cl<sub>2</sub> will deactivate the carbon (Fig. 2a).<sup>[1]</sup> By measuring the amount of Cl<sub>2</sub> adsorbed/ desorbed on carbon at a temperature in a temperature programmed desorption, the reversibility and the nature of  $Cl_2$ interaction with carbon are examined. Fig. 2b shows the setup to evaluate the activated carbon's Cl<sub>2</sub> adsorption capacity since those parameters give important hints for catalytic

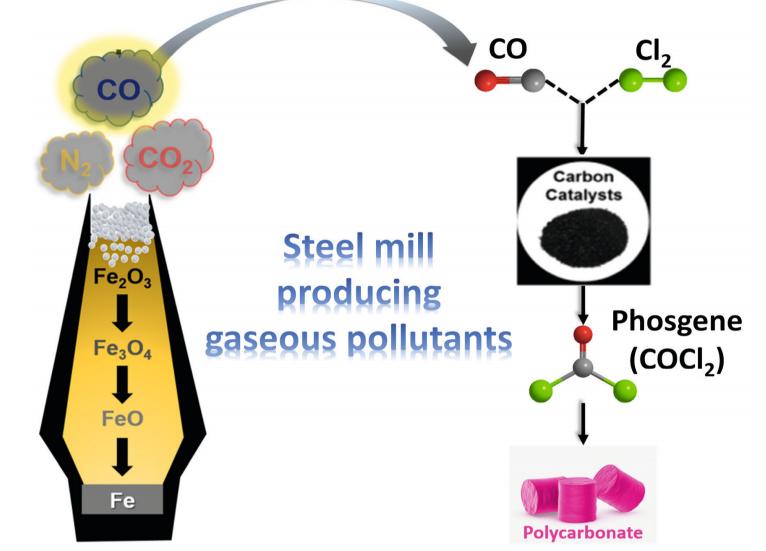
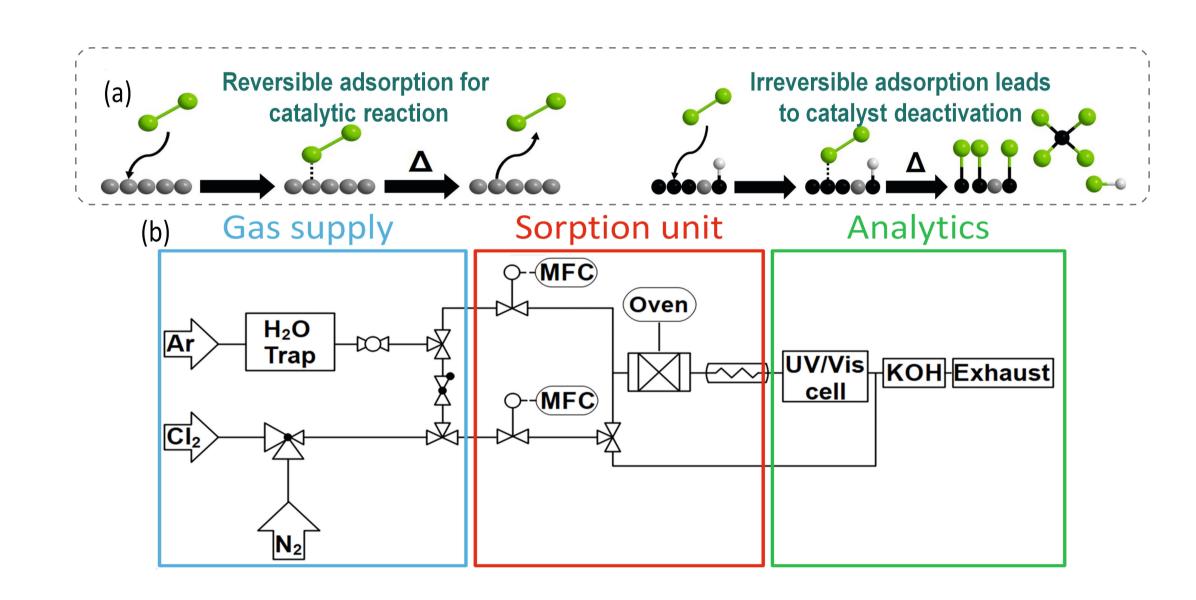


Fig. 1: Steel mill exhaust CO gas conversion to polycarbonate.

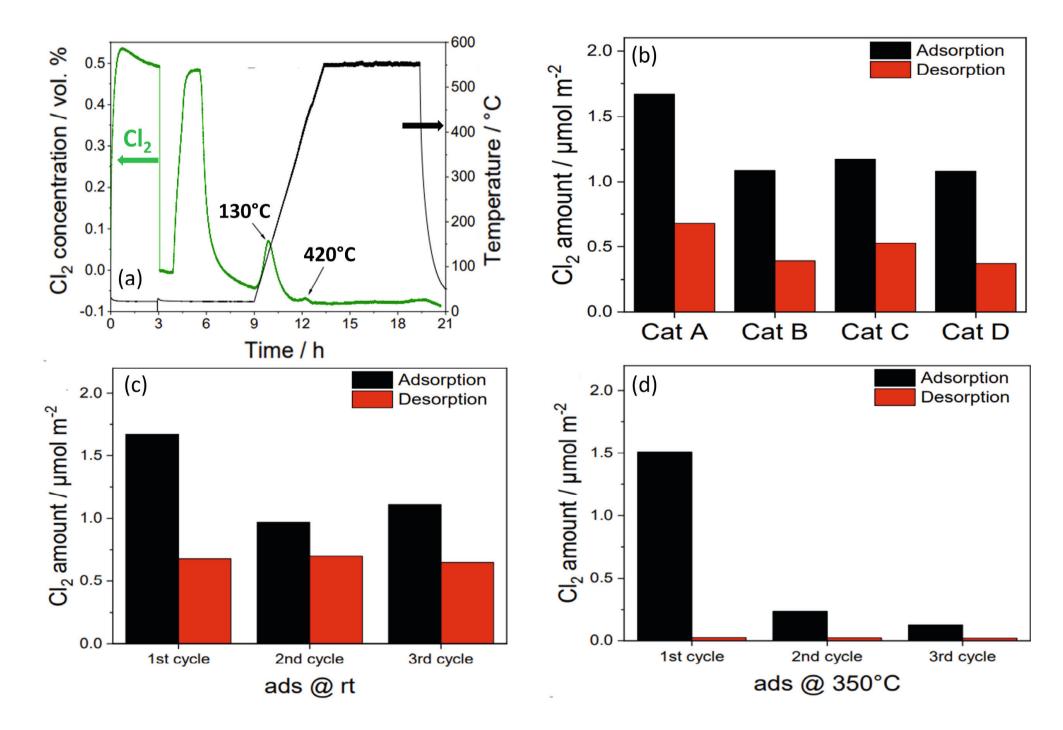


#### performance.<sup>[2]</sup>

## **ACTIVITY/STABILITY TESTING OF ACT. CARBON**

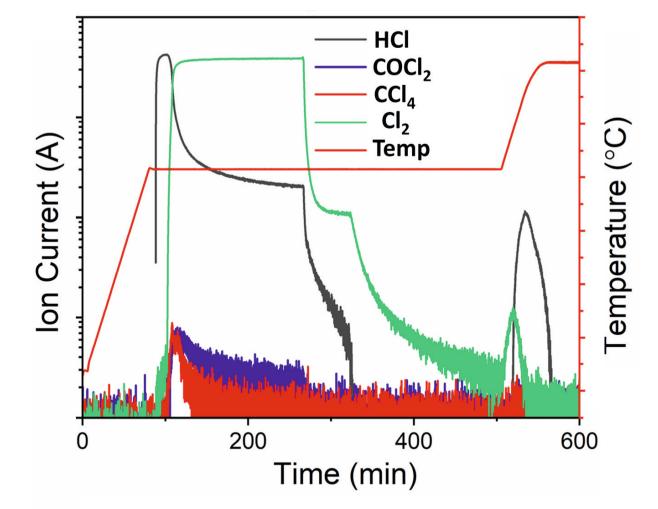
The Cl<sub>2</sub> adsorption/desorption experiment is carried out in tubular bed reactors over activated carbons (A-D). Fig. 3a shows the concentration of Cl<sub>2</sub> gas adsorbed at RT and desorbed at a higher temperature on Cat A. Compared to other carbons, Cat A exhibits a higher amount of Cl<sub>2</sub> adsorption/ desorption, along with stable  $CI_2$  desorption over 3 cycles at RT (Fig. 3b,c). At higher temperature, the adsorbed Cl<sub>2</sub> decreases over cycle test, and desorbed Cl<sub>2</sub> is negligible (Fig. 3d). The lack of balance between the adsorbed and desorbed Cl<sub>2</sub> suggests the loss of Cl<sub>2</sub> gas in the side reactions, hence, deactivating the catalysts.

**Fig. 2:** (a) Scheme for reversible and irreversible Cl<sub>2</sub> adsorption on graphitic (left) and non-graphitic (right) carbon. (b) Set-up for Cl<sub>2</sub> interaction analysis. <sup>[3]</sup>



**Fig. 3:** (a) Cl<sub>2</sub> concentration during adsorption/desorption at RT on Cat A. (b) Amount of Cl<sub>2</sub> adsorbed/desorbed at RT on Cat A, B, C and D. Cycling test at (c) RT and (d) 350 °C on Cat A.<sup>[3]</sup>

#### Gaseous products analysis



### **WORK PROGRESS AND OUTLOOK FOR PHASE II**

- (i) Gaseous side products analysis using quadrupole mass analyzer produced during Cl<sub>2</sub> adsorption exp. on activated carbon (Fig. 4).
- (ii) In situ Raman spectroscopy to investigate the changes in

#### In situ structure analysis

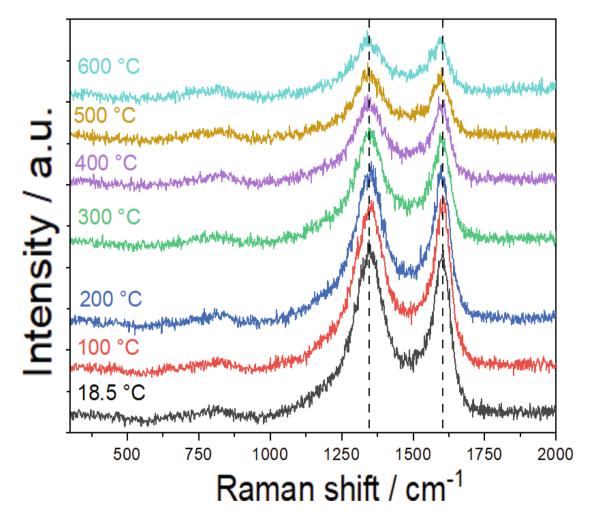


Fig. 4: Gases evolved during Cl<sub>2</sub> experiment.

the carbon structure under the Cl<sub>2</sub> atmosphere at a particular temperature (Fig. 5).

#### References

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- A. Bähr, G.-h. Moon, J. Diedenhoven, J. Kiecherer, E. Barth, H. Tüysüz, Chem. Ing. Tech. 2018, 90, 1513–1519.
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### Fig. 5: Carbon structure change during Cl<sub>2</sub> experiment.

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